

Carisma 2012 – Copenhagen

3<sup>rd</sup>-5<sup>th</sup> September

# Electrocatalytic activity and stability of antimony doped tin oxide supported platinum catalyst for PEM fuel cells

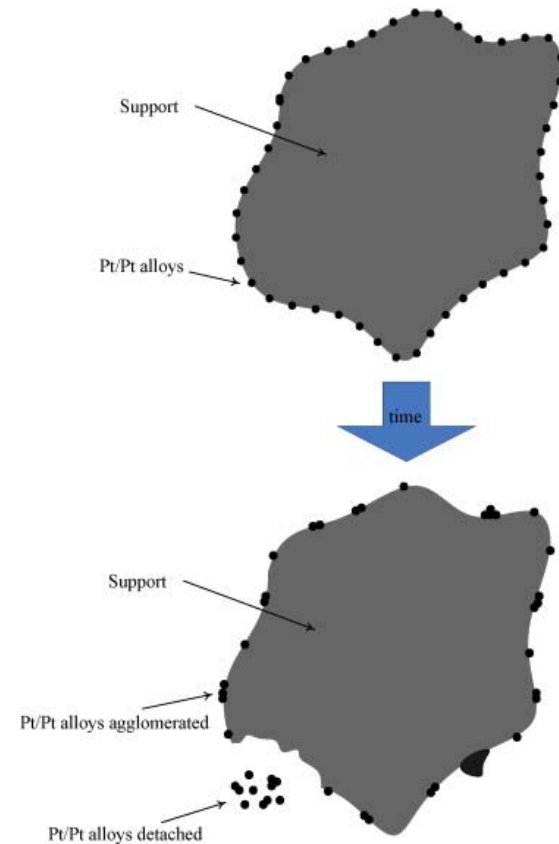
Magnus Thomassen, Luis Colmenares, Edel Sheridan

SINTEF Materials and Chemistry

Trondheim, Norway

# Introduction

- Catalyst degradation is one of the main causes of reduction of PEM fuel cell performance
- Loss of catalyst active surface area
  - Sintering, dissolution/precipitation
- Corrosion of catalyst support
  - Loss of catalyst/support contact
  - Changes in surface chemistry
  - Collapse of catalyst layer
  - Reduction in conductivity/connectivity of electronic pathways.



Yuyan Shao , Geping Yin , Yunzhi Gao  
Journal of Power Sources Volume 171, Issue 2 2007 558 - 566

# Background

- Several FCH-JU projects on PEM fuel cell degradation
- High competence on synthesis of complex oxides
- Previously developed a highly active Ir/ATO catalyst for PEM electrolyzers.
- Initial trials for development of oxide supported Pt catalysts

STAYERS



Linked to Danish  $\mu$ CHP project



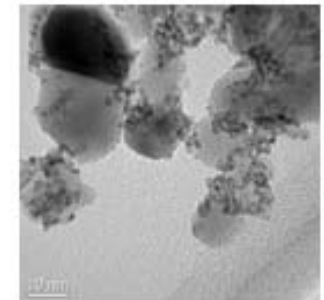
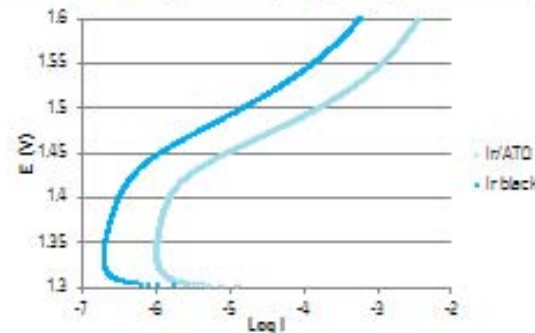
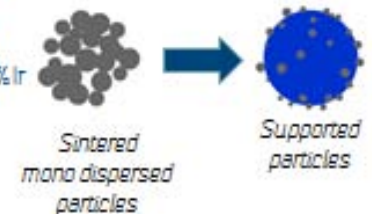
KEEPERALIVE aims to establish:

STAYERS



## Technical highlights – catalyst materials

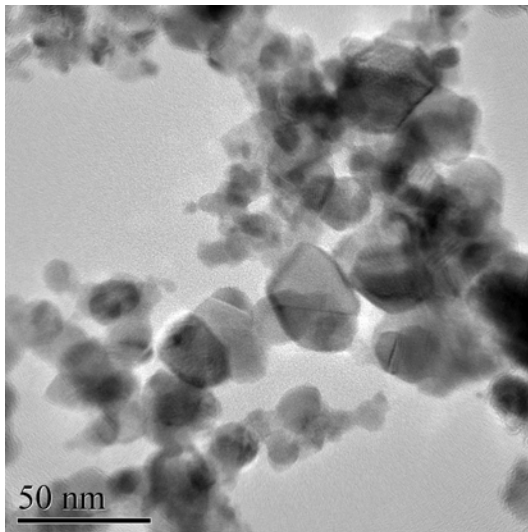
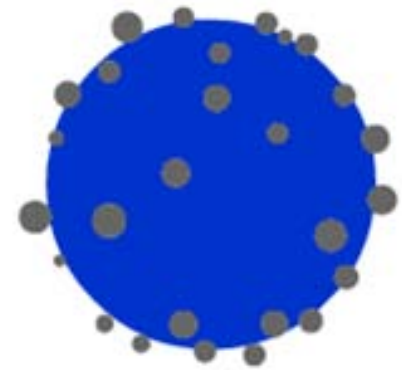
- Highly active oxygen evolution catalysts developed
  - 2 nm Ir particles on Antimony Tin Oxide support (20wt% Ir)
  - 200% higher activity than state of the art catalysts (0.94 Acm<sup>-2</sup> at 1.65 V and 80 °C)
  - Scaled up synthesis (~30 g catalyst batch size)



NEXPEL - Next-Generation PEM Electrolyser for Sustainable Hydrogen Production

# Targeted catalyst composition and morphology

- Platinum nanoparticles (d ~ 2-4 nm)
- Antimony doped Tin Oxide as support
- Platinum loading of 20 wt%
- Polyol method selected for synthesis
  - Gives small particle size and narrow size distribution



BET surface area : 37 m<sup>2</sup>g<sup>-1</sup>

Particle size: 10-50 nm

Doping level: 7-11 % Sb

High stability in acidic media and at elevated potentials

Relatively high electronic conductivity (> 10<sup>-3</sup> S cm<sup>-1</sup>)

# Experimental – Synthesis (Polyol Method)

## 1. Isolate Platinum

Reflux Pt-precursor

pH adjusted EG solution

high temperature

## 2. Add support

Antimony Tin Oxide

well dispersed

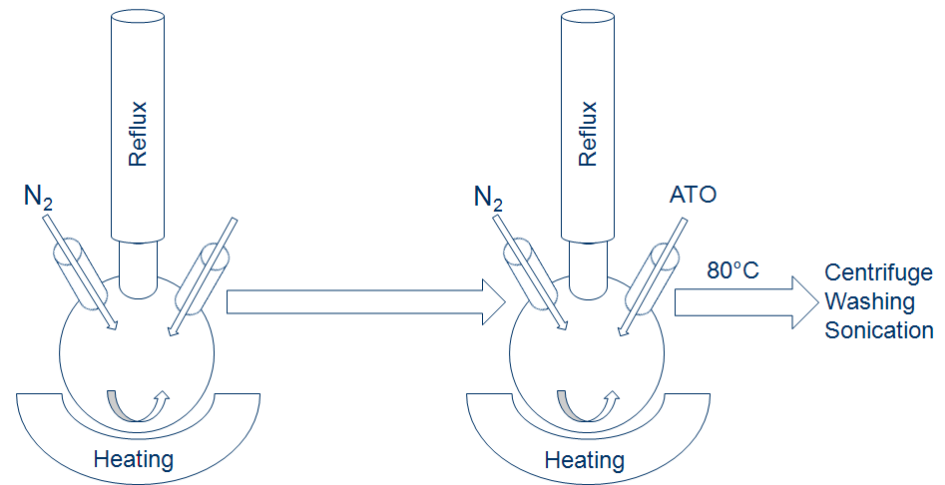
reflux lower temperature

Adjust pH

## 3. Isolate catalyst

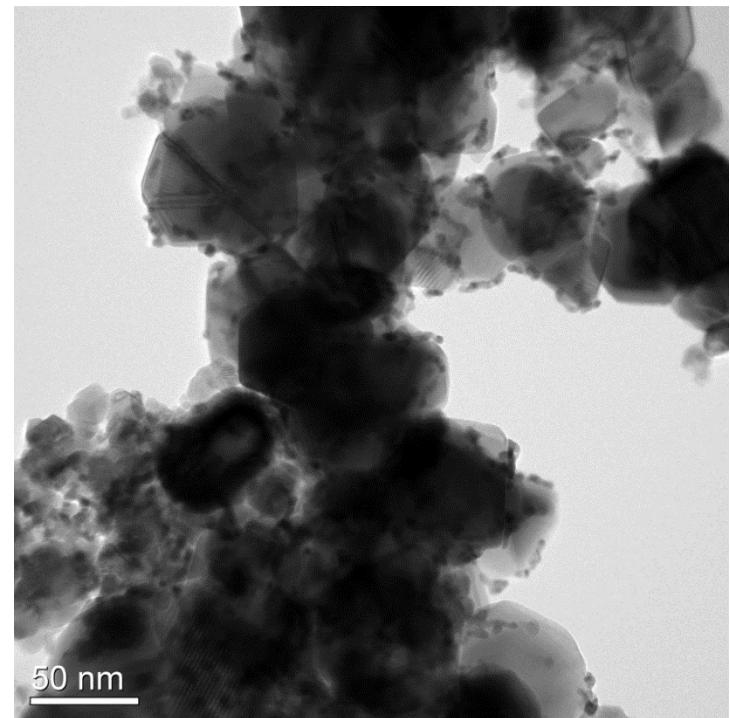
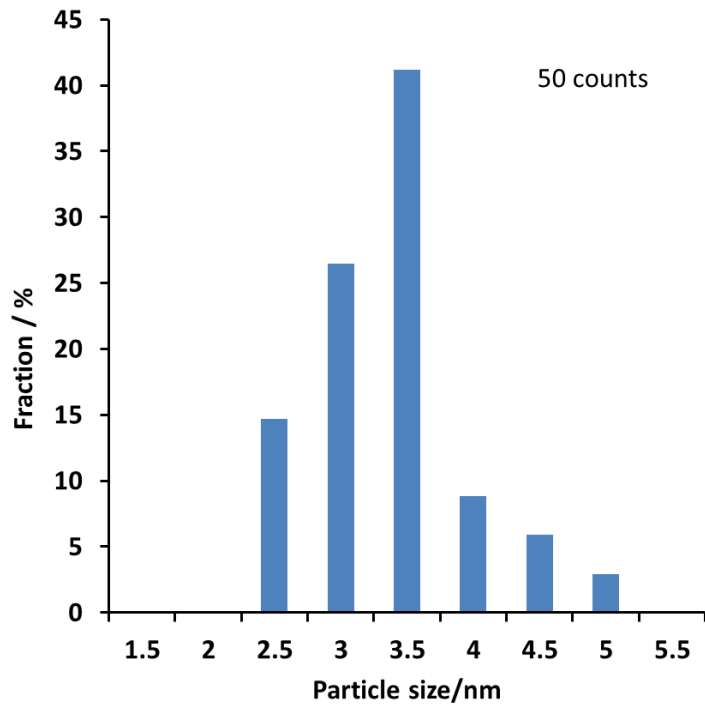
Centrifuge to remove EG

Sonicate and rinse until pH is that of rinsing water



# TEM analysis

- Average particle size 3.2 nm
- Well dispersed on ATO surface



# Thin-film Working Electrode Preparation

## 1. Aqueous catalyst suspension ( $1 \text{ mg}_{\text{CAT}} / \text{ml}$ )

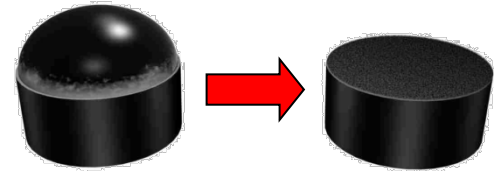


Only Milli-Q water (pH 7)

50/50 Water/iso-propanol (pH 5-6)

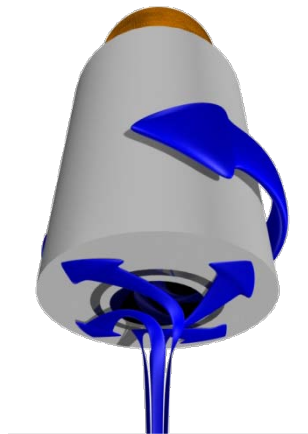
Milli-Q water at pH 3

## 2. Thin-film electrode



1.  $20 \mu\text{l}$  of catalyst suspension
2. Dry under Ar atmosphere
3.  $20 \mu\text{l}$  of 0.05 wt.% Nafion
4. Dry under Ar atmosphere

Catalyst deposited =  $20 \pm 3(7\%) \mu\text{g}$

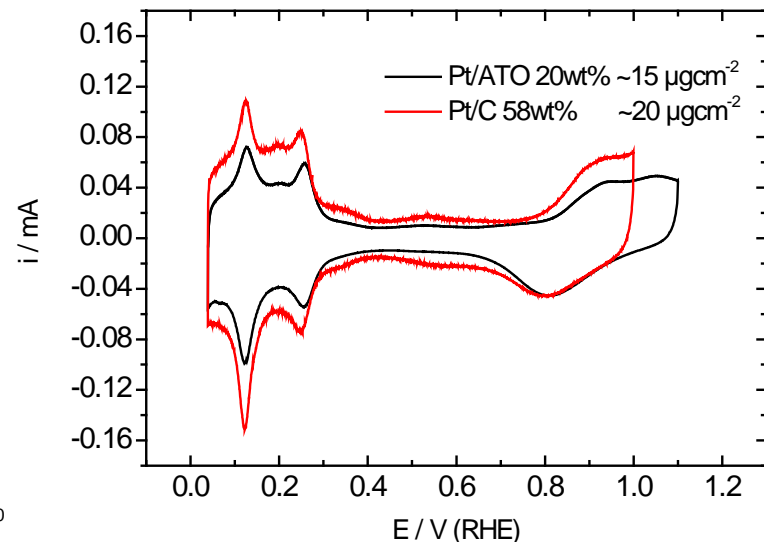
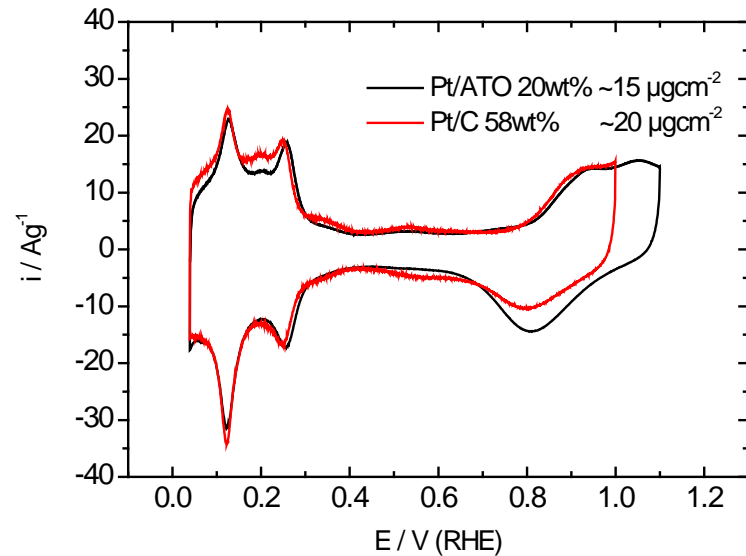
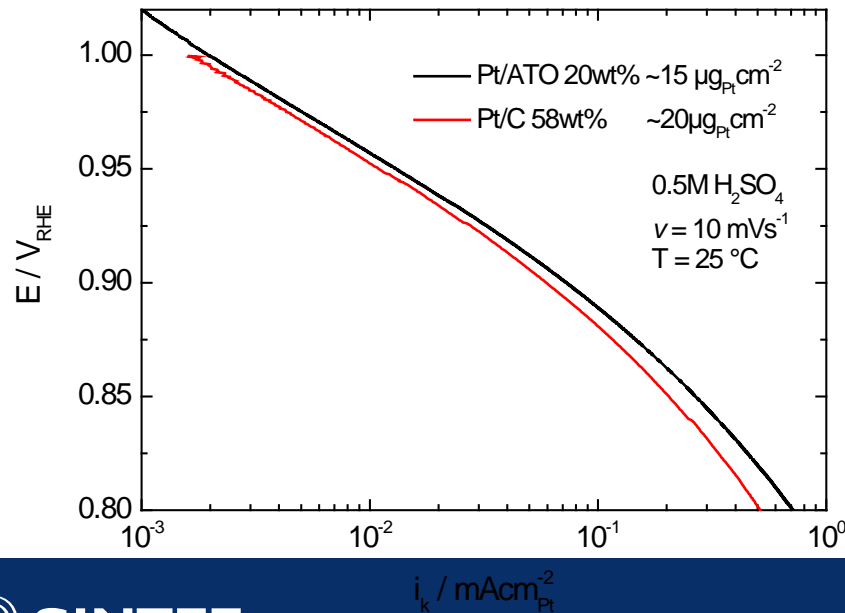


## 3. Rotating Disk Electrode

(Pine Instrument) is used for performing the electrochemical measurements in  $0.5 \text{ M H}_2\text{SO}_4$  electrolyte  
geometric area:  $0.196 \text{ cm}^2$

# Pt/ATO vs Pt/C

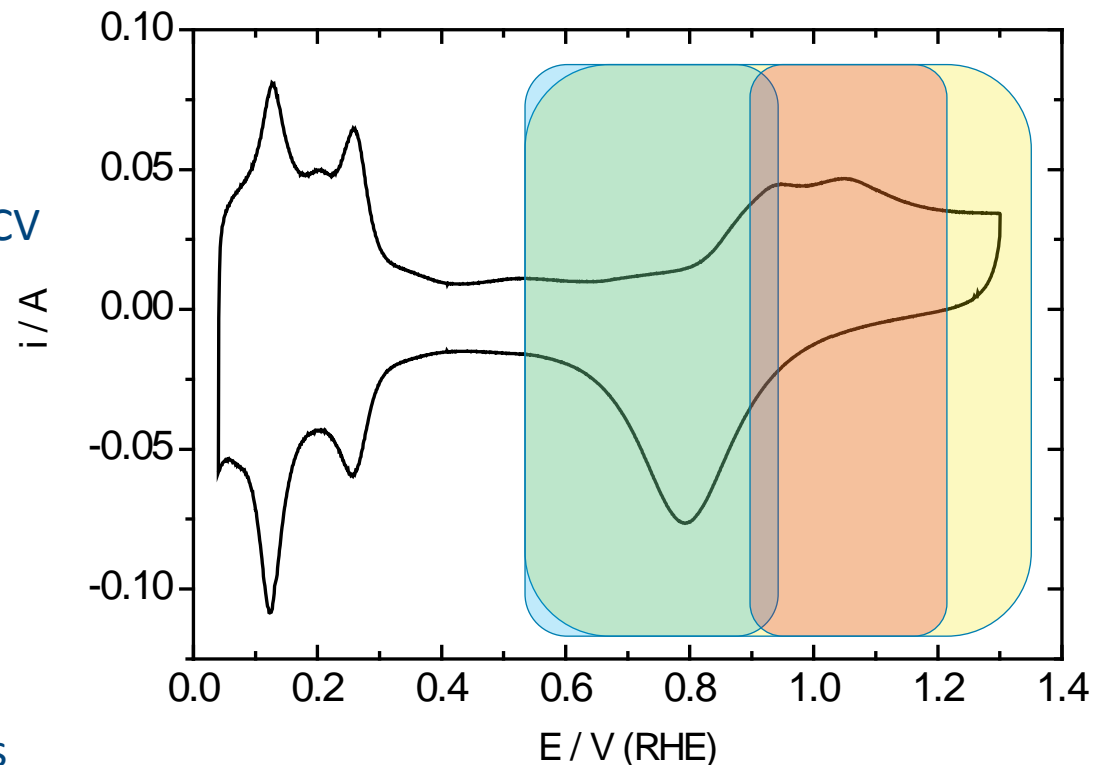
- Comparison of fresh catalyst with commercial 58wt% Pt/C
  - 15 $\mu\text{g}$  20wt% Pt/ATO & 20 $\mu\text{g}$  58 wt% Pt/C gives roughly same electrode thickness
  - ECSA and catalytic activity very similar (107 & 106  $\text{cm}^2\text{g}^{-1}$ )





# AST Protocols

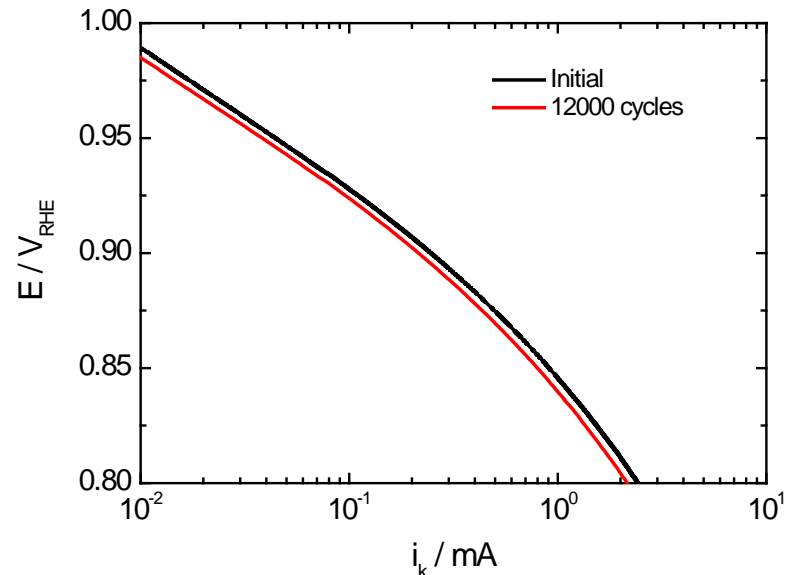
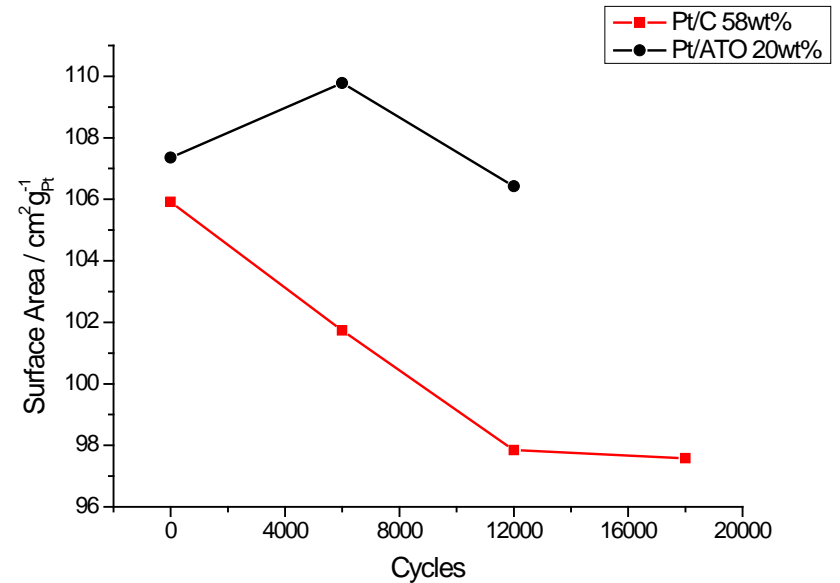
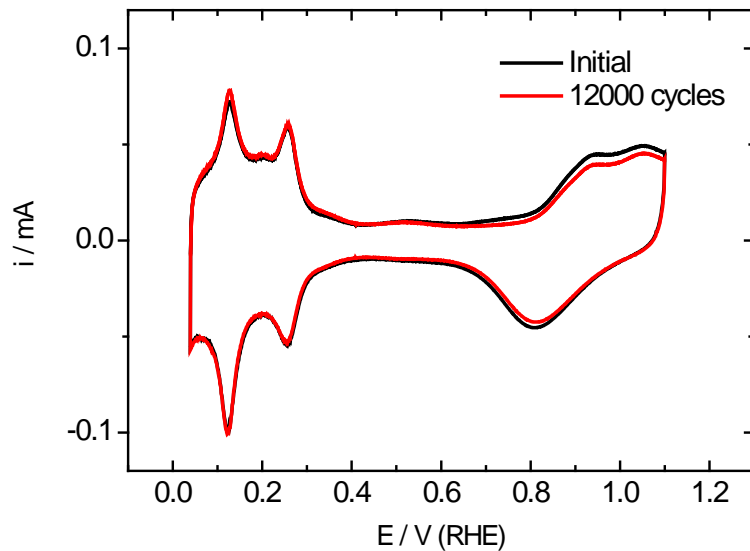
- Catalyst stability evaluated against three different AST protocols
- Load cycling (0.55-0.95V):
  - Mimic normal FC operation.
  - Pt catalyst in reduced state
- Start up (0.9-1.2V):
  - Elevated potentials due to OCV and gas purge
  - Catalyst in oxidized state
- Shut down (0.55-1.35V)
  - Elevated potentials due to gas purge
  - Catalyst cycled between reduced and oxidised state
  - Elevated carbon corrosion rates



# Results - Load cycling

0.55V-0.95V  
800 mVs<sup>-1</sup>  
12000/18000 cycles

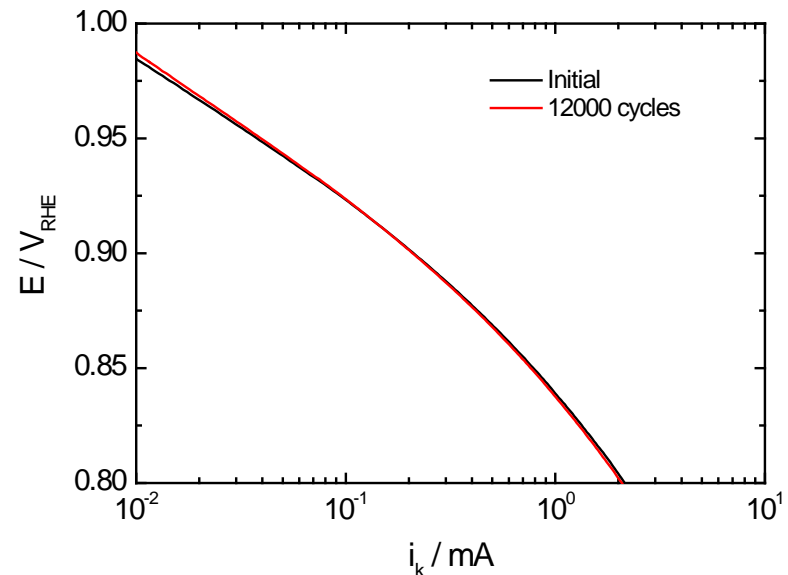
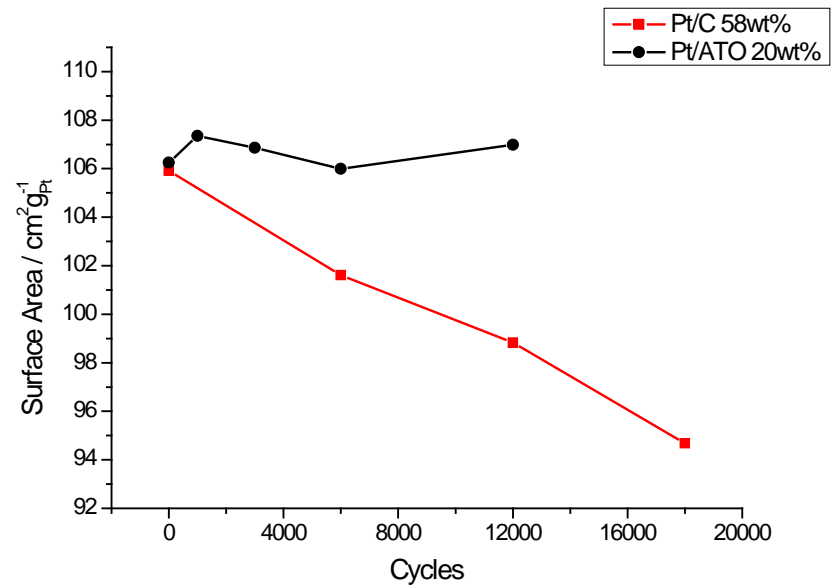
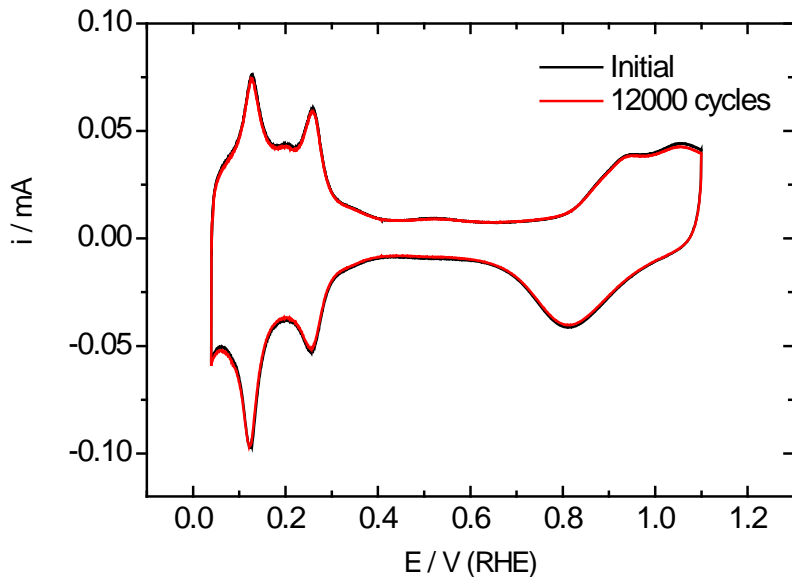
- Pt/ATO show no change in ECSA or ORR activity
- Pt/C ECSA reduced by 8%



# Results - Start Up

0.9V-1.2V  
800 mVs<sup>-1</sup>  
12000/18000 cycles

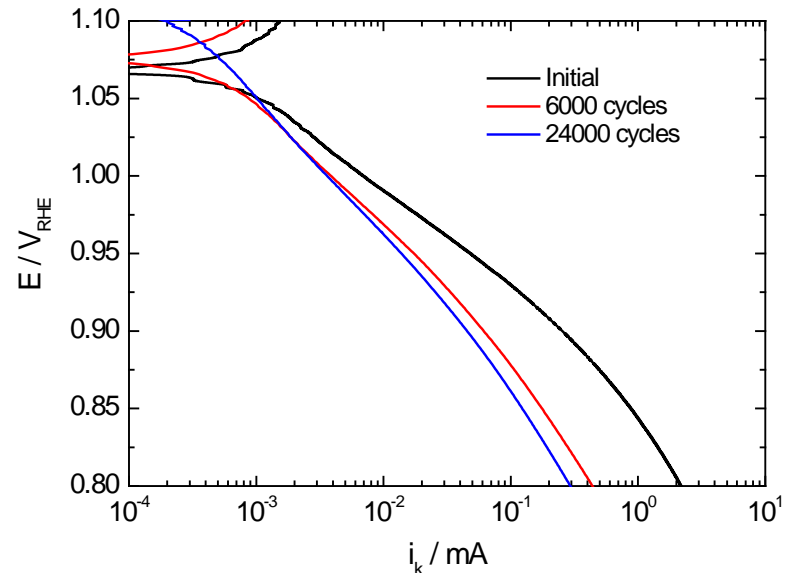
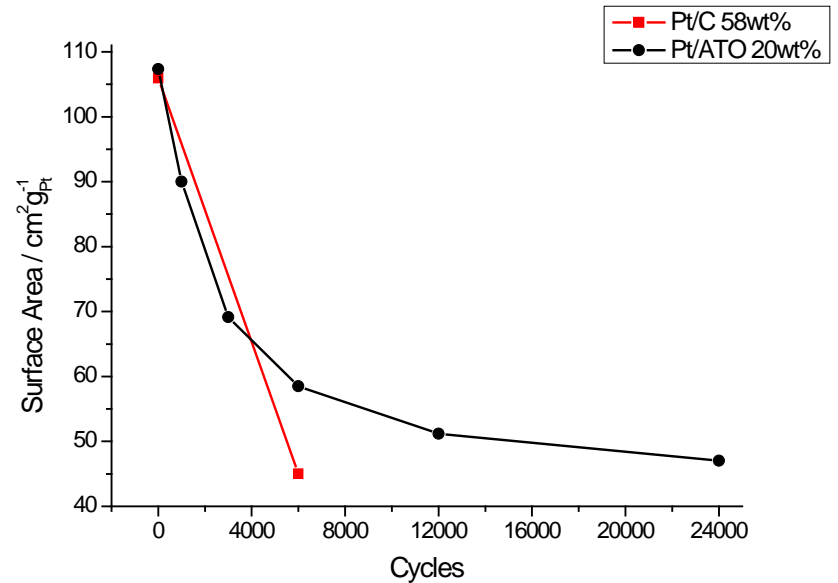
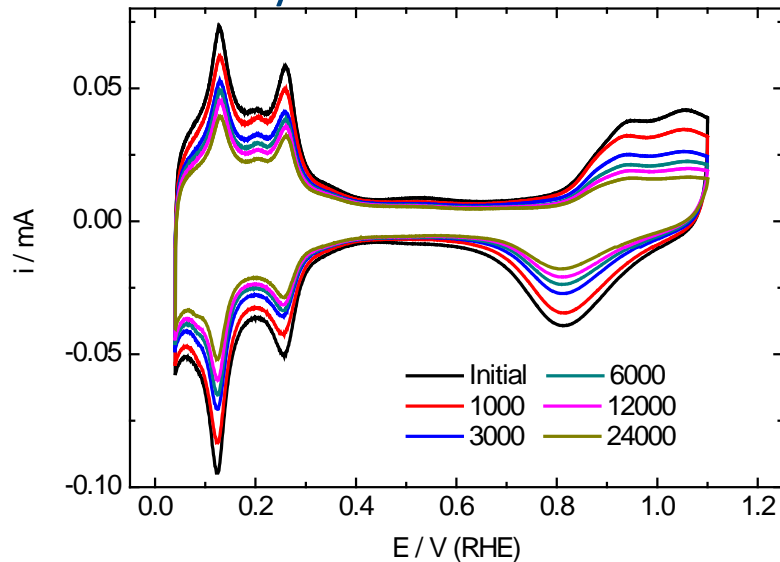
- Pt/ATO show no change in ECSA or ORR activity
- Pt/C ECSA reduced by 12%



# Results - Shut Down

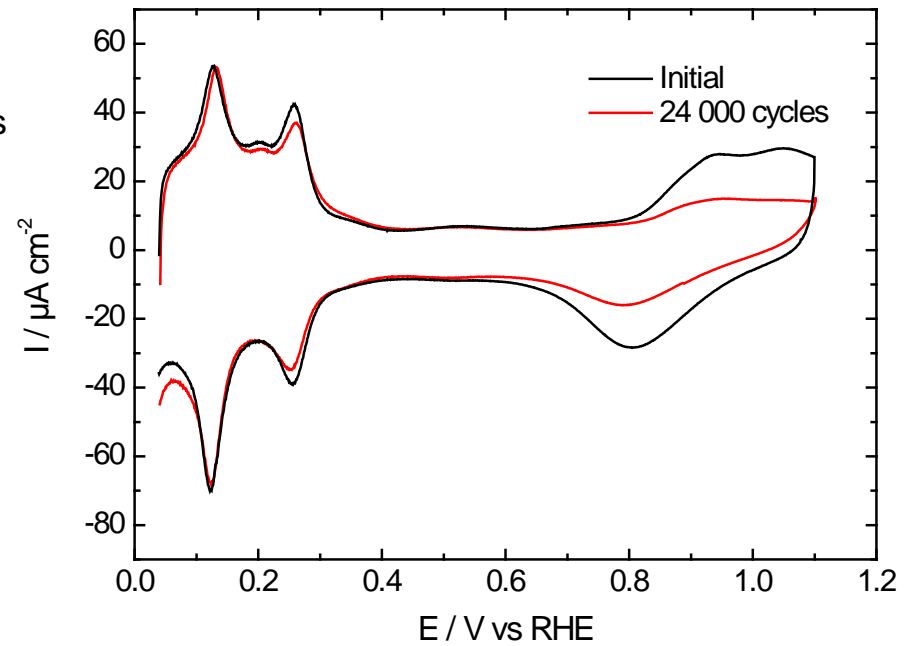
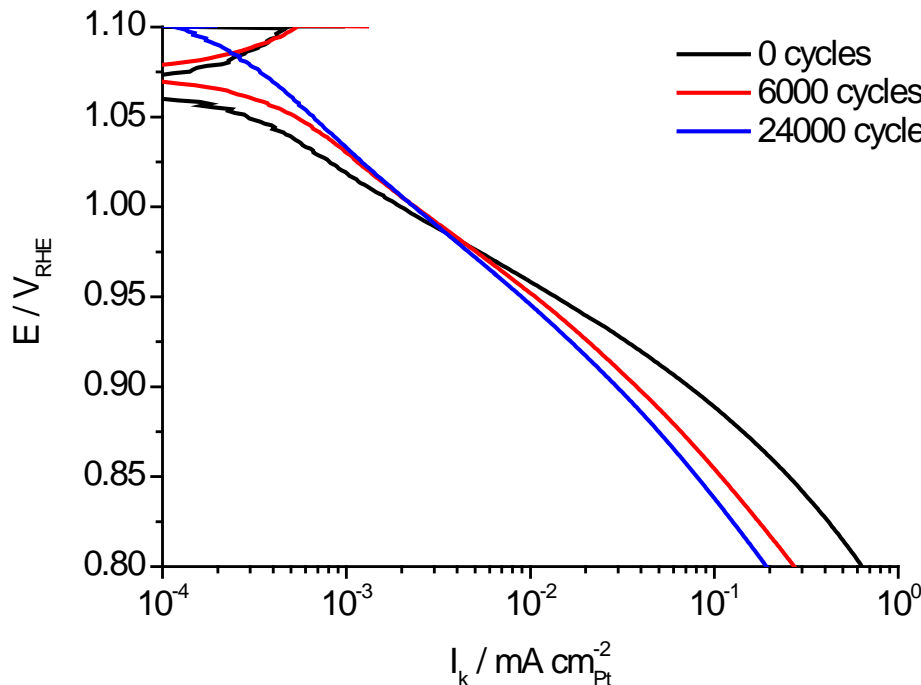
0.55-1.35 (Pt/ATO)  
0.6-1.2V (Pt/C)  
800 mVs<sup>-1</sup>  
24000/5000 cycles

- Pt/ATO ECSA reduced by 55% after 24000 cycles
- Pt/C ECSA reduced by 60% after 5000 cycles



# Shut Down – normalised results against ECSA

- ORR specific activity ( $\text{mA cm}^{-2}$ ) increases at  $E > 1\text{V}$  with repeated cycling of Pt/ATO catalyst
- Tafel slope changes from  $\sim 60$  to  $\sim 80$  mV/dec
- Pt oxidation is significantly retarded after potential cycling.
  - Pt-Sb alloy formation? , Increased interaction between Pt and ATO-support?



# Conclusions

- Pt/ATO catalyst successfully synthesized
  - Well dispersed, 3.5nm Pt particles on ATO support
- Catalyst ORR activity and ECSA similar to commercial Pt/C
- Increased stability towards AST protocols compared to Pt/C
  
- Repeated cycling of Pt/ATO catalyst to elevated voltages (>1.2 V) causes significant increase of oxygen reduction activity at voltages above 1V.
  - Cause of reduction in Pt oxidation still unclear
  
- In situ fuel cell measurements and studies using model electrodes are planned.
  - Comments and cooperation are welcome!

Thank you for your attention

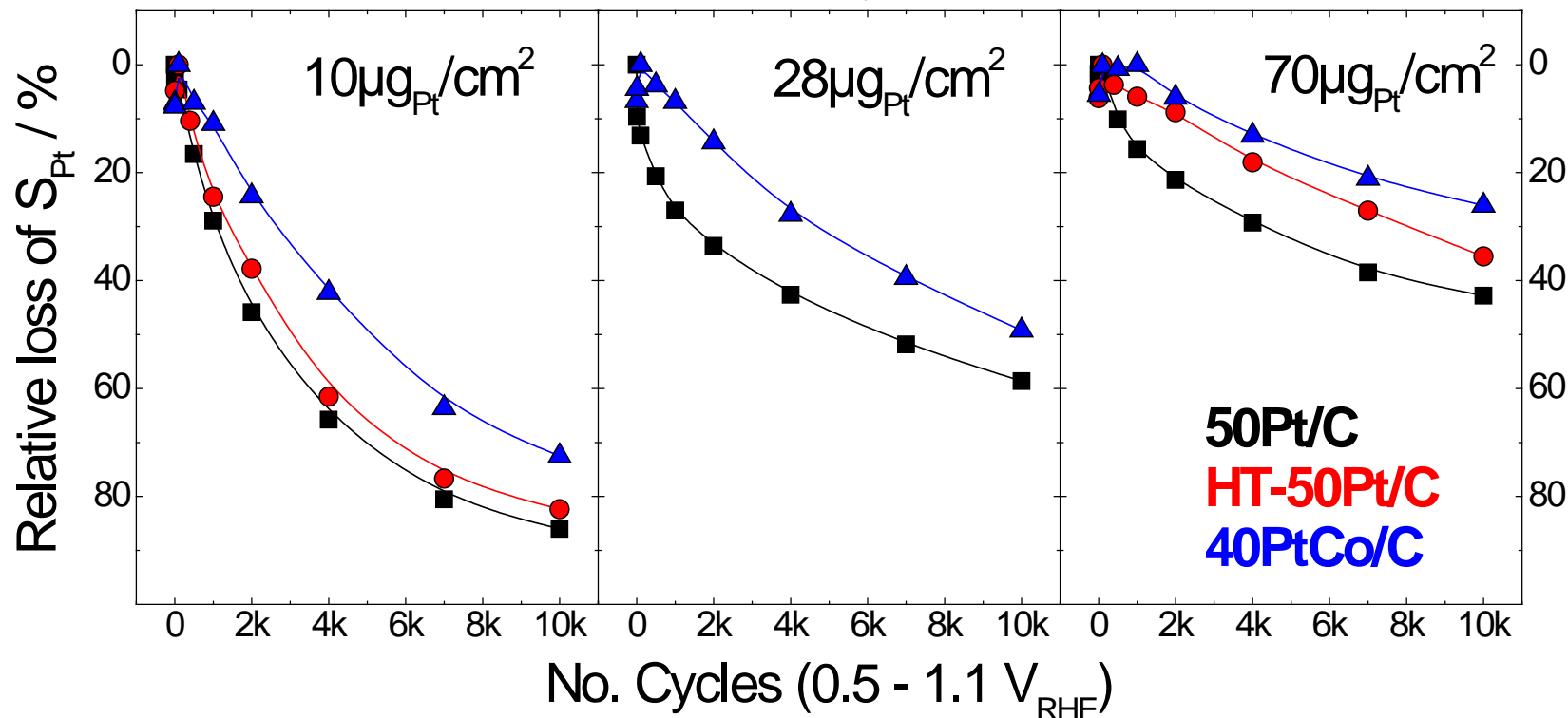


# Supporting slides



# ADT – Active Pt Surface Area Loss

- Relative ECSA loss as a function of catalyst thin-film (CTF) thickness

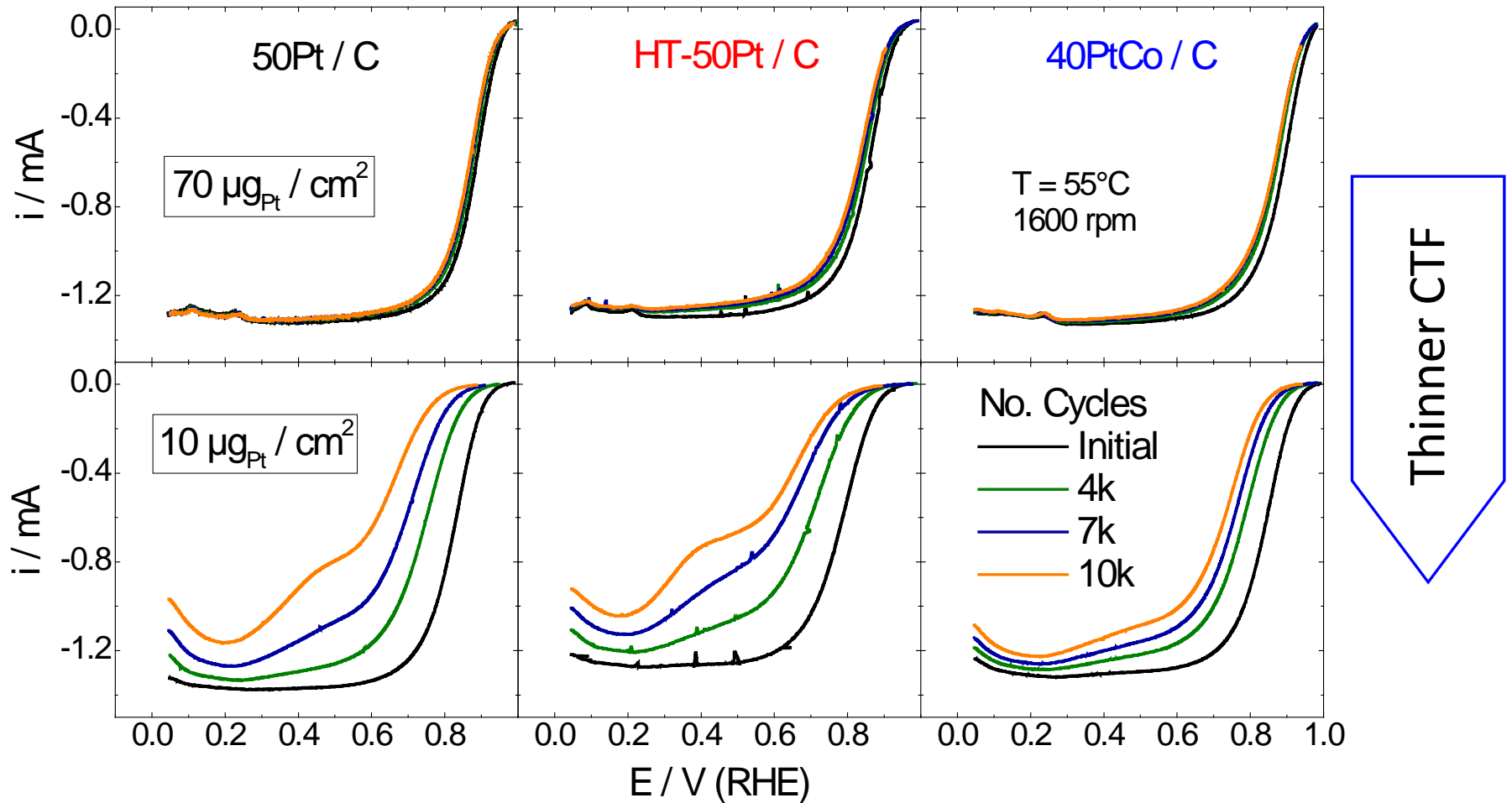


ECSA loss depends on

- CTF thickness, particle size and catalyst composition
- Thinner CTF  $\rightarrow$  smaller probability of Pt redeposition
- Larger particle size  $\rightarrow$  slows down particle growth  $\rightarrow$  smaller ECSA loss
- $Pt_3Co/C$   $\rightarrow$  smaller relative loss of ECSA in comparison to Pt/C catalysts

# ADT – ORR Characteristics

- ORR Activity as a function of catalyst thin-film (CTF) thickness



Thinner CTF → significant decrease in ORR Activity